



上海交通大学
SHANGHAI JIAO TONG UNIVERSITY



Introduction to Marine Hydrodynamics

(NA235)

Department of Naval Architecture and Ocean Engineering

School of Naval Architecture, Ocean & Civil Engineering

Shanghai Jiao Tong University



Second Assignment

- ◆ The assignment can be downloaded from following website:

Website: <ftp://public.sjtu.edu.cn>

Username: dcwan

Password: 2015mhydro

Directory: IntroMHydro2015-Assignments

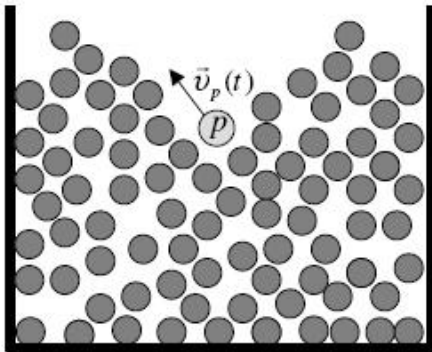
- ◆ Eight problems
 - ◆ Submit the assignment on March 19th (in English, written on paper)
-



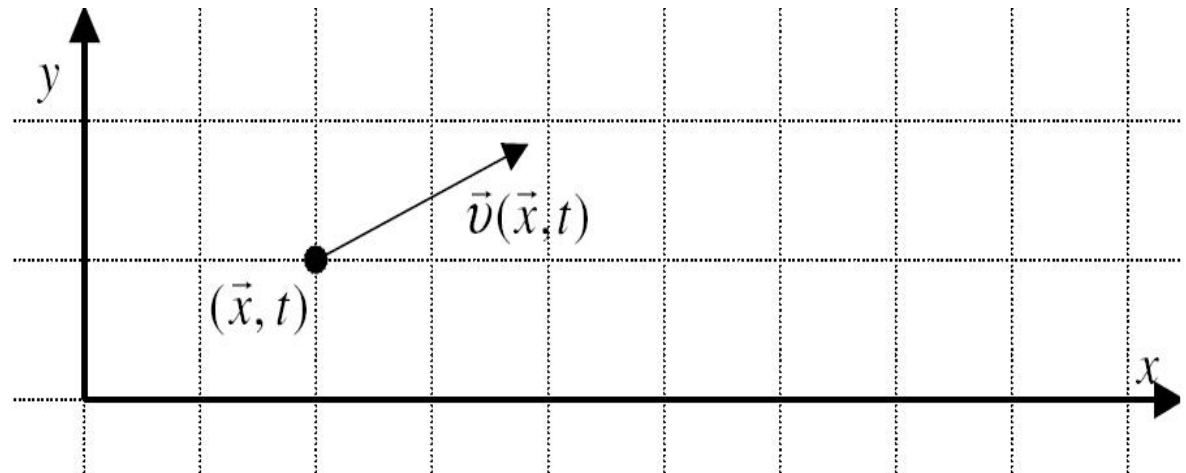
Review

Two ways of describing a fluid flow:

Lagrangian description, Eulerian description



Lagrangian description; snapshot



Eulerian description; Cartesian grid



Review: Differences between Lagrangian and Eulerian Descriptions

Differences:

Particle positions x, y, z in Lagrangian description; while spatial point (x, y, z) in Eulerian description.

Spatial point (x, y, z) in Eulerian description is **independent** variable of t , however, particle positions x, y, z in Lagrangian description are **functions** of t .



Review

● Total (material, substantial) derivative:

$$\frac{D(\quad)}{Dt} = \frac{\partial(\quad)}{\partial t} + (\mathbf{v} \cdot \nabla)(\quad)$$

Effects of the unsteadiness
of the flow

Effects of the fluid particle moving
(advecting or convecting) to a new
location in the flow, where the
velocity field is different



2.2 Pathlines and Streamlines

Various ways to visualize flow fields —

- ◆ Pathlines
- ◆ Streamlines

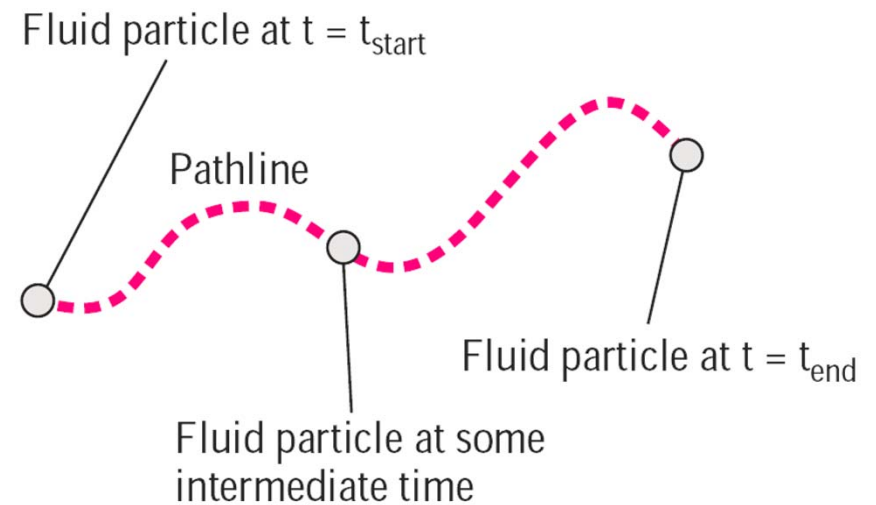


2.2.1 Pathlines

Definition: a **pathline** is the **trajectory** of a fluid particle of fixed identity over a period of time.

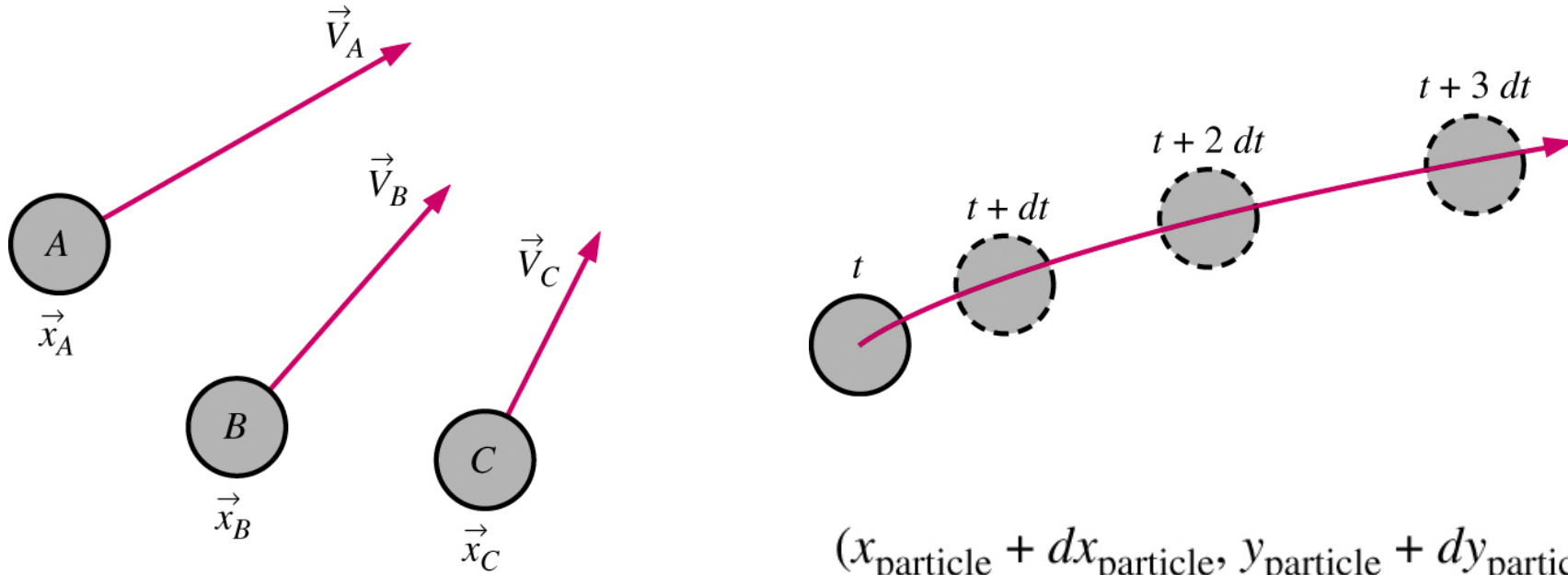
As pathlines are the actual paths traveled by individual fluid particles over some time period. In **Lagrangian description**, a pathline is the same as the fluid particle's **position vector**:

$$\begin{cases} x = x(a, b, c, t) \\ y = y(a, b, c, t) \\ z = z(a, b, c, t) \end{cases}$$

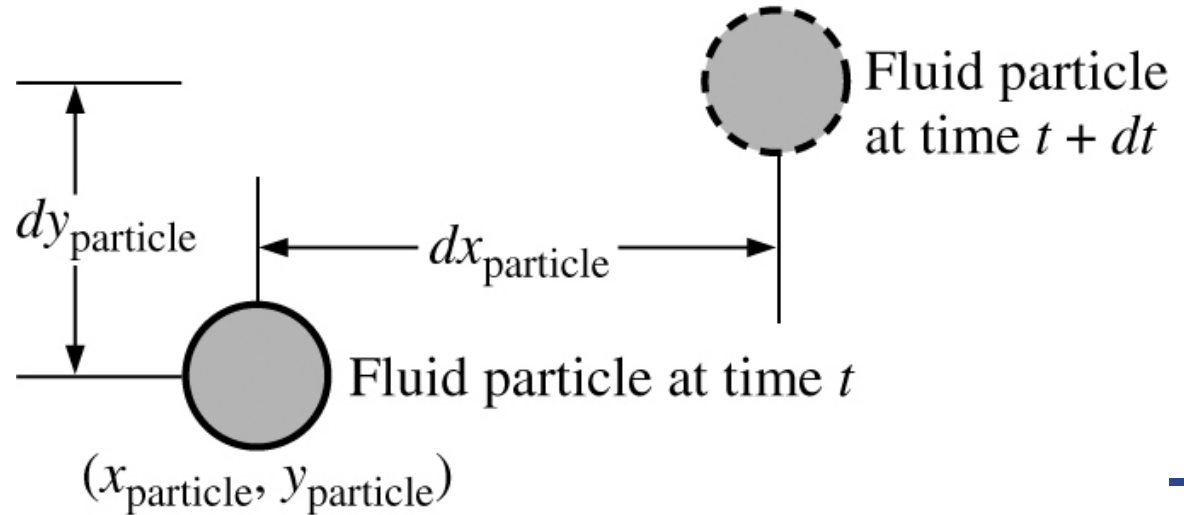




2.2.1 Pathlines

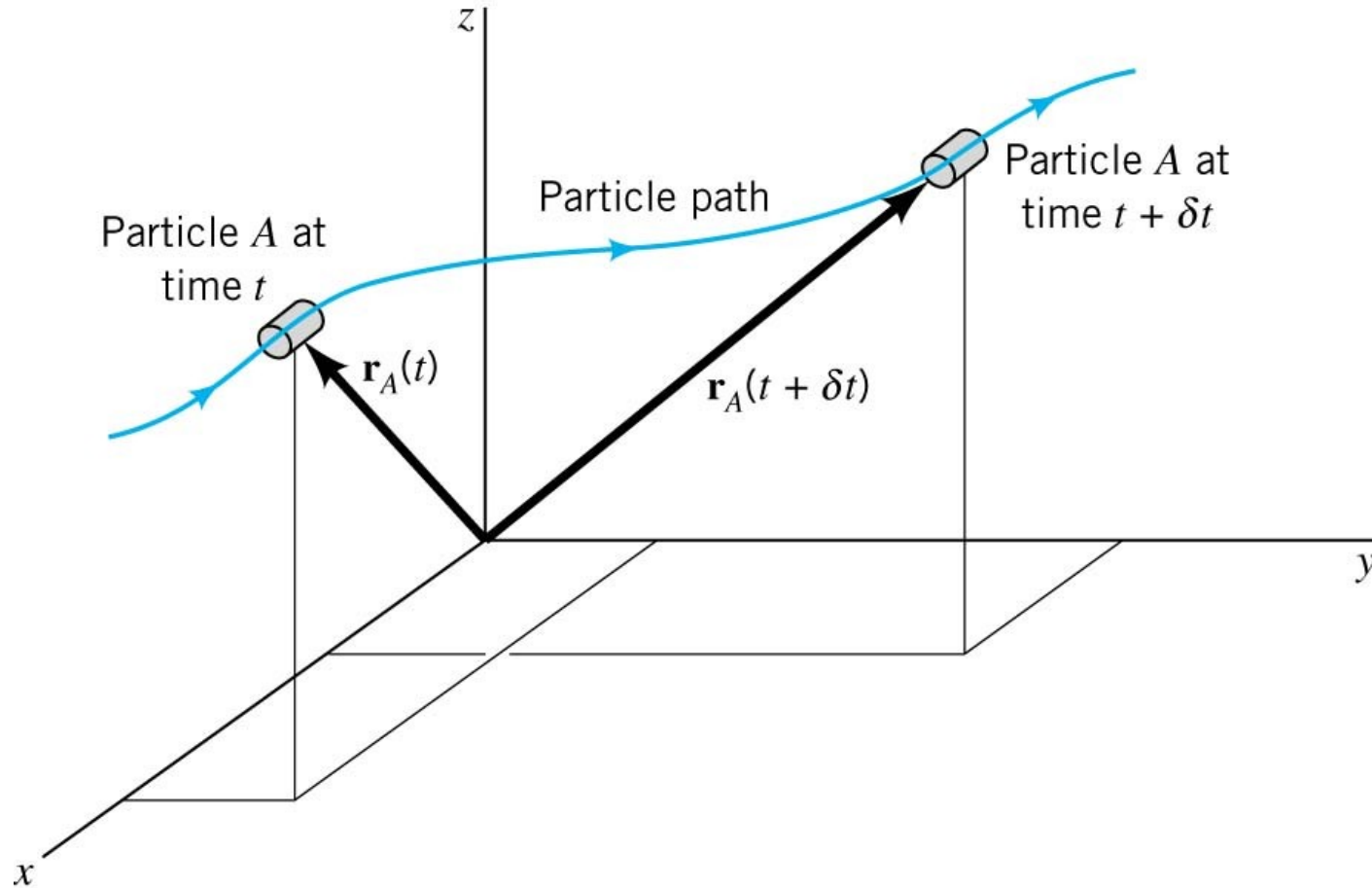


$$(x_{\text{particle}} + dx_{\text{particle}}, y_{\text{particle}} + dy_{\text{particle}})$$



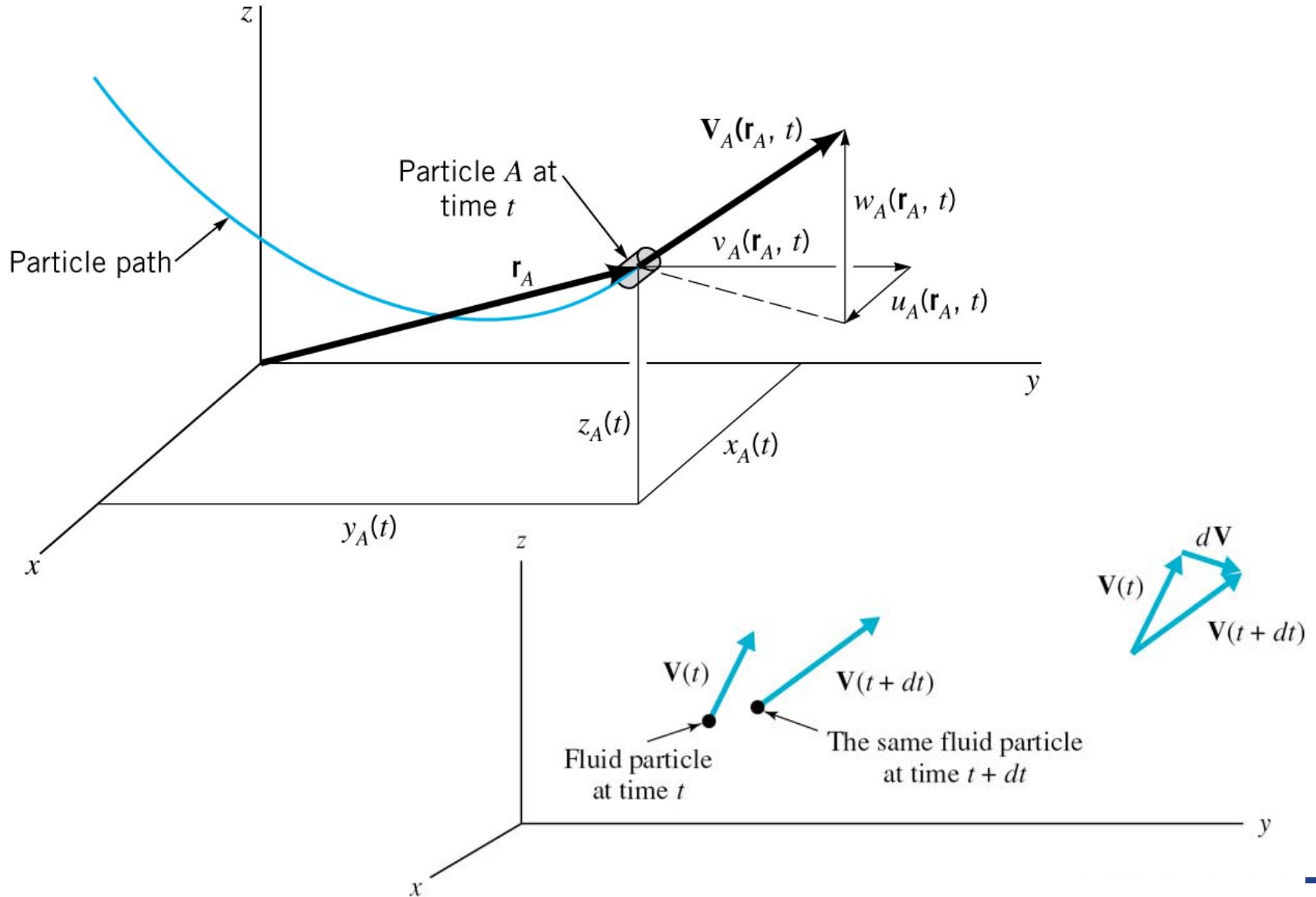


2.2.1 Pathlines





2.2.1 Pathlines





2.2.1 Pathlines

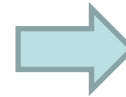
Normally, the velocity field is given by Eulerian description as:

$$\mathbf{V} = \mathbf{V}(\mathbf{r}, t) = \mathbf{V}(x, y, z, t)$$

A fluid particle moves from one spatial position (x, y, z) to another $(x+u dt, y+v dt, z+w dt)$ over a period of time dt , i.e., it moves a distance of $d\mathbf{r}$. The equation of the **pathline** for the fluid particle is:

$$d\mathbf{r} = \mathbf{V} dt$$

or written as



x, y, z are functions of t

$$\begin{cases} \frac{dx}{dt} = u \\ \frac{dy}{dt} = v \\ \frac{dz}{dt} = w \end{cases}$$

$$\frac{dx}{u} = \frac{dy}{v} = \frac{dz}{w} = dt$$

Since the pathline is defined by **integration** of the relationship between velocity and displacement, to integrate (u, v, w) with respect to t , use initial condition (x_0, y_0, z_0, t_0) to determine the integral constants, then eliminate t .



2.2.2 Streamlines

Definition: a **streamline** is a curve that is **everywhere tangent** to the velocity vector **at a given instant.**

At an instant of time, there is at every point a velocity vector with a definite direction. The instantaneous curves that are everywhere **tangent** to the **direction** field are called the **streamlines** of flow.



2.2.2 Streamlines

Two-dimensional flows

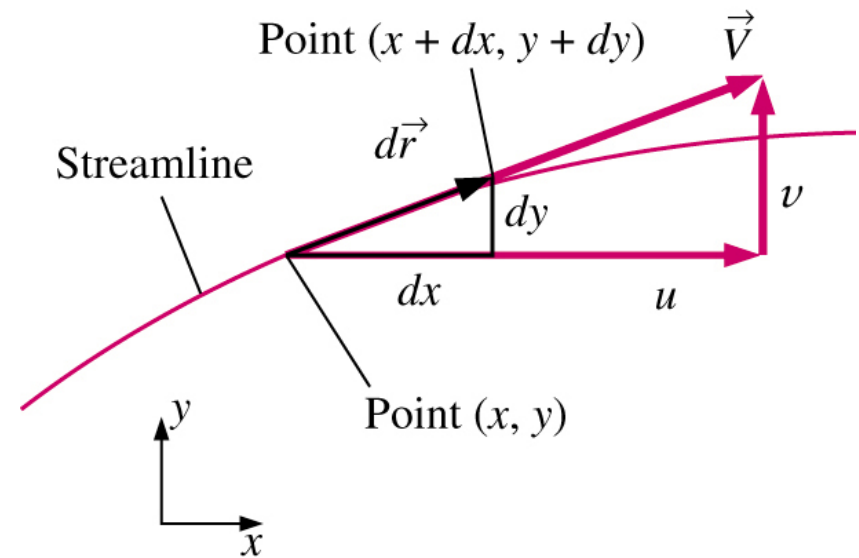
By definition, the local velocity vector \mathbf{V} and the element of arc length along a streamline $d\mathbf{r}$ are locally **parallel**, thus the equation for a streamline is:

$$\mathbf{V} \times d\mathbf{r} = 0$$

$$\frac{dx}{u} = \frac{dy}{v} = \frac{dz}{w}$$

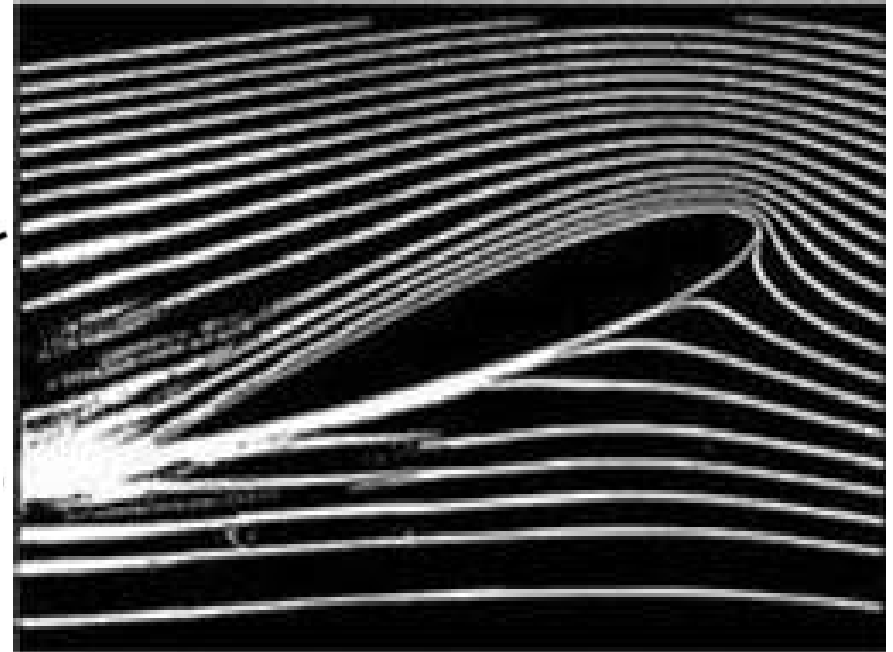
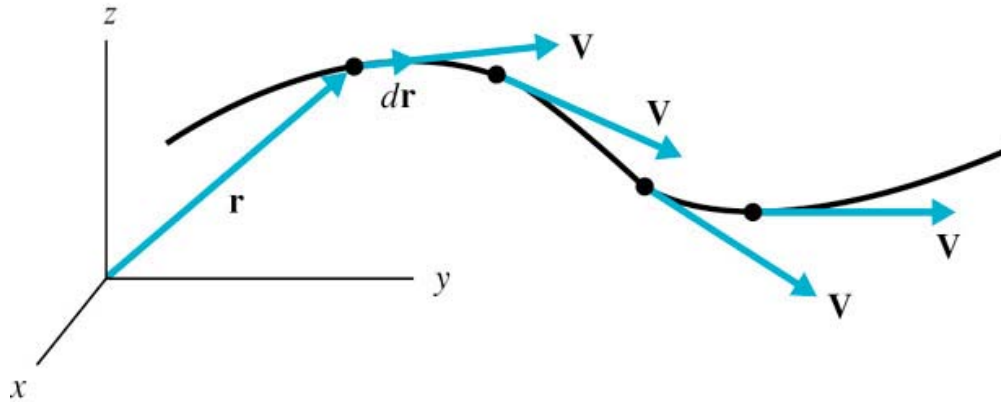
Also by simple geometric arguments using similar triangles, the slope of the streamline:

$$\frac{dy}{dx} = \frac{v}{u}$$





2.2.2 Streamlines



$$\mathbf{V} \times d\mathbf{r} = 0$$

Pathlines and streamlines are identical in steady flows



2.2.2 Streamlines

Characteristics of streamlines:

- ◆ Instantaneous quantities
- ◆ Tangential direction of the streamlines are **identical** to the velocity vectors. Streamline cluster density reflects the magnitude of velocity: streamlines **close** together \Rightarrow **high** velocity, streamline **far apart** \Rightarrow **low** velocity
- ◆ The streamlines **never intersect** each other except at a point of **zero** velocity, because at any point, there can be only one direction of the velocity
- ◆ The streamlines **never interrupt** in the fluid
- ◆ Since the velocity vector in the flow field is everywhere **tangent** to the streamline, the fluid **cannot cross** the streamlines and the streamlines can be regarded as fixed walls

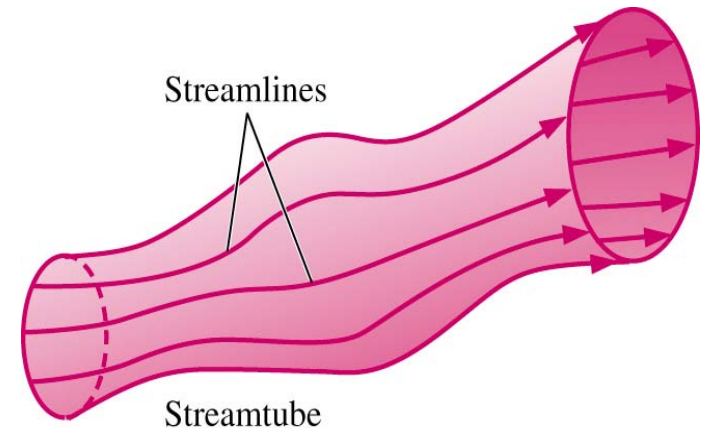


2.2.2 Streamlines

Streamtube

Definition: a set of streamlines that intersect a closed loop in space.

Streamtubes are instantaneous quantities like streamlines, defined at a particular instant in time according to the velocity field at that instant. When the flow is steady, the shape of the streamtube does not change with t , like a real pipe. **No** fluid crosses a stream tube's surface because the fluid velocity vector is everywhere **tangent** to it.



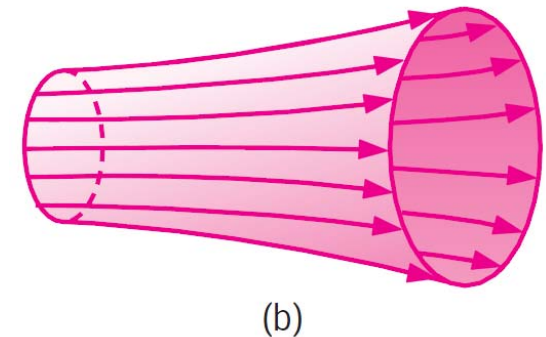
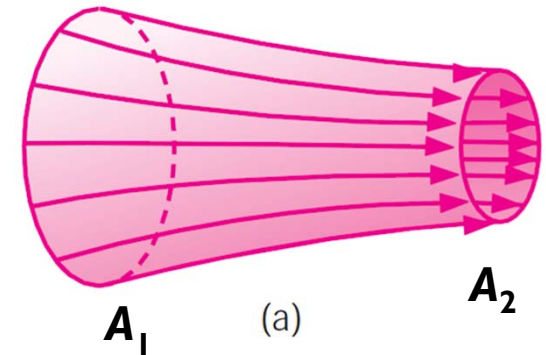


2.2.2 Streamlines

Streamtube

Let's take **two cross-sections** of a streamtube, with cross-sectional areas A_1 and A_2 . The velocities **perpendicular** to the cross-sections are V_1 and V_2 , respectively. The rate at which **mass** is entering the streamtube is $\rho_1 A_1 V_1$; the rate at which it is leaving is $\rho_2 A_2 V_2$. If the flow is **steady**, the mass is conserved and then $\rho_1 A_1 V_1 = \rho_2 A_2 V_2$, and if flow is **incompressible**, then $A_1 V_1 = A_2 V_2$.

The fluid speed **increases** when the cross-sectional area of the streamtube **decreases**.



In an incompressible flow field, a streamtube (a) **decreases** in diameter as the flow **accelerates** or converges and (b) **increases** in diameter as the flow **decelerates** or diverges.



2.2.2 Streamlines

Flux

Definition: the flow rate of a property (volume, mass, weight) per unit area of a **spatial curved surface** **per unit of time** — volumetric **flux**, mass **flux**, weight **flux**.

Volumetric flux: the rate of volume flow across a unit area

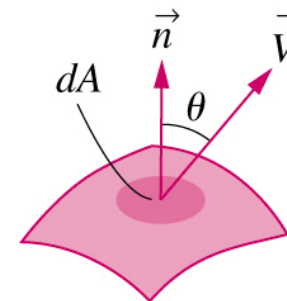
$$Q_1 = \iint_S v_n ds = \iint_S \mathbf{V} \cdot \mathbf{n} ds$$

Mass flux: the rate of mass flow per unit area

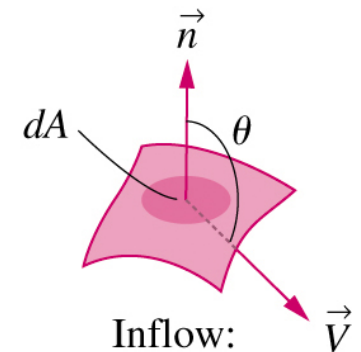
$$Q_2 = \iint_S \rho v_n ds$$

Weight flux: the rate of weight flow per unit area

$$Q_3 = \iint_S \rho g v_n ds$$



Outflow:
 $\theta < 90^\circ$



Inflow:
 $\theta > 90^\circ$

For a closed surface S, take the unit outer normal as positive, then the flux is:

$$\vec{V} \cdot \vec{n} = |\vec{V}| |\vec{n}| \cos \theta = V \cos \theta$$

If $\theta < 90^\circ$, then $\cos \theta > 0$ (outflow).

If $\theta > 90^\circ$, then $\cos \theta < 0$ (inflow).

If $\theta = 90^\circ$, then $\cos \theta = 0$ (no flow).

$$\oiint_S (\rho \mathbf{V} \cdot \mathbf{n}) dS = \iiint_\Omega \nabla \cdot (\rho \mathbf{V}) d\Omega$$

Gauss' theorem



Application1: Pathlines and Streamlines

A two-dimensional velocity field is given as: $u = \frac{x}{1+t}$, $v = y$

(1) Determine the pathline equation for $(x)_{y=1, t=0} = 1$

(2) Determine the streamline equation for $(x)_{t=0} = a$, $(y)_{t=0} = b$

Solution: (1)

The pathline equation is: $\frac{dx}{dt} = \frac{x}{1+t}$, $\frac{dy}{dt} = y$

Integrating to give: $\ln x = \ln(t+1) + \ln C_1$, $\ln y = t + \ln C_2$

i.e., $x = C_1(1+t)$, $y = C_2 e^t$

From $(x)_{y=1, t=0} = 1$: $C_1 = 1$, $C_2 = 1$

Thus, the pathline equation is:
$$\begin{cases} x = 1+t \\ y = e^t \end{cases}$$



上海交通大学 Application 1: Pathlines and Streamlines

Shanghai Jiao Tong University

(2) The streamline equation is: $\frac{1+t}{x} dx = \frac{1}{y} dy$

Integrating, yield: $(1+t) \ln x = \ln y + \ln C$

i.e., $x^{1+t} = Cy$

From $(x)_{t=0} = a$, $(y)_{t=0} = b$: $C = \frac{a}{b}$

Thus, the streamline equation at $t=0$ and (a, b) is: $y = \frac{b}{a}x$



Application2

Assume the pathline equation of a fluid particle is:

$$x = C_1 e^t - t - 1$$

$$y = C_2 e^t + t - 1 \quad \text{where } C_1, C_2, C_3 \text{ are constant}$$

$$z = C_3$$

- Determine:**
- (1) The pathline equation of the fluid particle at $x=a$, $y=b$, $z=c$, and $t=0$;
 - (2) The velocity of any fluid particle;
 - (3) The expression of velocity field by Eulerian description;
 - (4) Are the acceleration field by Eulerian description and the acceleration field by converting Lagrangian description to Eulerian description the same?



Solution: (I) The pathline equation

Substituting $t = 0, x = a, y = b, z = c$ into the pathline equation, yields:

$$a = C_1 - 1, \quad b = C_2 - 1, \quad c = C_3$$

Thus, $C_1 = a + 1, \quad C_2 = b + 1, \quad C_3 = c$

The pathline equation of the fluid particle at (a, b, c) is:

$$\begin{aligned} x &= (a + 1)e^t - t - 1 \\ y &= (b + 1)e^t + t - 1 \\ z &= c \end{aligned} \tag{I}$$

**(2) The velocity of any fluid particle:**

$$u = \frac{\partial x}{\partial t} = C_1 e^t - 1 = (a + 1)e^t - 1$$

$$v = \frac{\partial y}{\partial t} = C_2 e^t + 1 = (b + 1)e^t + 1 \quad (2)$$

$$w = \frac{\partial z}{\partial t} = 0$$



(3) Expressing the velocity field by Eulerian description

a, b, c are solved from Equation (1):

$$\begin{aligned}a &= \frac{1}{e^t}(x+t+1) - 1 \\b &= \frac{1}{e^t}(y-t+1) - 1 \\c &= z\end{aligned}\quad (3)$$

Substituting into Equation (2), yields:

$$\begin{aligned}u &= \frac{\partial x}{\partial t} = (a+1)e^t - 1 = x+t \\v &= \frac{\partial y}{\partial t} = (b+1)e^t + 1 = y-t+2 \\w &= \frac{\partial z}{\partial t} = 0\end{aligned}\quad (4)$$



(4) Determining the acceleration field by Eulerian description

$$a_x = \frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z} = x + t + 1$$

$$a_y = \frac{\partial v}{\partial t} + u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} + w \frac{\partial v}{\partial z} = y - t + 1$$

$$a_z = \frac{\partial w}{\partial t} + u \frac{\partial w}{\partial x} + v \frac{\partial w}{\partial y} + w \frac{\partial w}{\partial z} = 0$$

From Equation (1), the acceleration of the particle at (a, b, c) is:

$$\begin{aligned} a_x &= \frac{\partial^2 x}{\partial t^2} = (a+1)e^t \\ a_y &= \frac{\partial^2 y}{\partial t^2} = (b+1)e^t \\ a_z &= \frac{\partial^2 z}{\partial t^2} = 0 \end{aligned} \quad (5)$$



Substituting Equation (3) to (5), yields:

$$a_x = x + t + 1$$

$$a_y = y - t + 1$$

$$a_z = 0$$

By comparison, the two results are the same



2.3 Deformation and Rotation of Fluid Elements

In theoretical mechanics, the motion of a rigid body can be split into the **translational motion** and the **rotational motion**.

$$\mathbf{V} = \mathbf{V}_M + \boldsymbol{\omega} \times \mathbf{r}$$

 \mathbf{V}_M

Velocity of a reference point M

 \mathbf{r}

Radius vector between a moving point and the reference point

 $\boldsymbol{\omega}$

Angular velocity



2.3 Deformation and Rotation of Fluid Elements

In fluid mechanics, to study the motion of the fluid, take a fluid element from the flow field. A point in this fluid element is $M(x, y, z)$, an adjacent point is $M'(x+dx, y+dy, z+dz)$. Let the velocity at M is \mathbf{V} , then the velocity at M' is:

$$\begin{aligned}
 \mathbf{V}_{M'} &= \mathbf{V}_M + \frac{\partial \mathbf{V}_M}{\partial x} \delta x + \frac{\partial \mathbf{V}_M}{\partial y} \delta y + \frac{\partial \mathbf{V}_M}{\partial z} \delta z + \dots \\
 &= \left(u + \frac{\partial u}{\partial x} dx + \frac{\partial u}{\partial y} dy + \frac{\partial u}{\partial z} dz \right) \mathbf{i} + (\dots) \mathbf{j} + (\dots) \mathbf{k} \\
 &= \left[\underbrace{u + \frac{\partial u}{\partial x} dx}_{(1)} + \underbrace{\frac{1}{2} \left(\frac{\partial u}{\partial y} - \frac{\partial v}{\partial x} \right) dy}_{(2)} + \underbrace{\frac{1}{2} \left(\frac{\partial u}{\partial z} - \frac{\partial w}{\partial x} \right) dz}_{(3)} \right. \\
 &\quad \left. + \underbrace{\frac{1}{2} \left(\frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right) dy}_{(4)} + \underbrace{\frac{1}{2} \left(\frac{\partial u}{\partial z} + \frac{\partial w}{\partial x} \right) dz}_{(5)} \right] \mathbf{i} + (\dots) \mathbf{j} + (\dots) \mathbf{k}
 \end{aligned}$$



2.3 Deformation and Rotation of Fluid Elements

In the equation:

$$(1) \quad \varepsilon_{xx} = \frac{\partial u}{\partial x} \quad \varepsilon_{yy} \quad \varepsilon_{zz}$$

$$(2) \quad \omega_z = -\frac{1}{2} \left(\frac{\partial v}{\partial x} - \frac{\partial u}{\partial y} \right)$$

$$(3) \quad \omega_y = \frac{1}{2} \left(\frac{\partial u}{\partial z} - \frac{\partial w}{\partial x} \right)$$

$$(4) \quad \varepsilon_{xy} = \frac{1}{2} \left(\frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right)$$

$$(5) \quad \varepsilon_{xz} = \frac{1}{2} \left(\frac{\partial u}{\partial z} + \frac{\partial w}{\partial x} \right)$$

ω_x

ε_{zy}



2.3 Deformation and Rotation of Fluid Elements

Physical meaning of each item in the equation

(I) Physical meaning of $\varepsilon_{xx} = \frac{\partial u}{\partial x}$, $\varepsilon_{yy} = \frac{\partial v}{\partial y}$, $\varepsilon_{zz} = \frac{\partial w}{\partial z}$



2.3 Deformation and Rotation of Fluid Elements

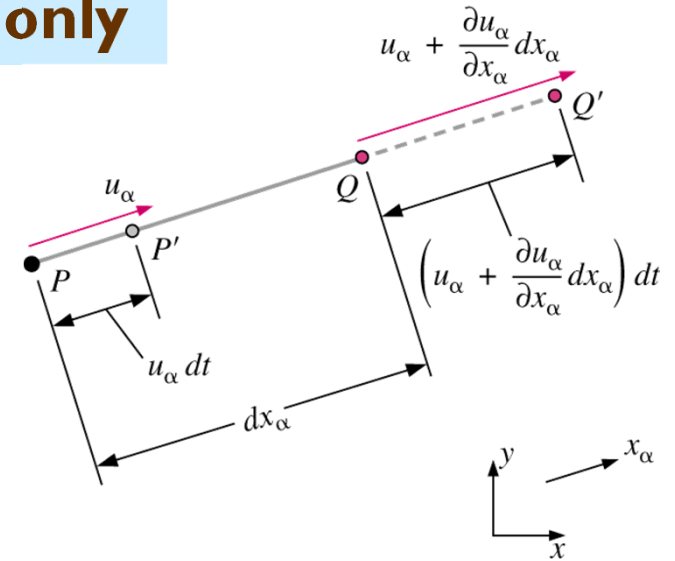
Consider the linear strain in x-direction only

Change of length per unit length:

$$\epsilon_x = \frac{\partial u}{\partial x} dx dt / dx = \frac{\partial u}{\partial x} dt$$

Rate of change of length per unit length:

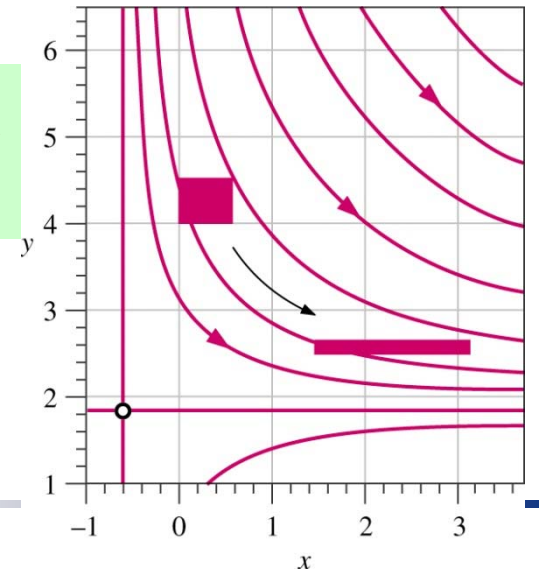
$$\epsilon_{xx} = \frac{\epsilon_x}{dt} = \frac{\partial u}{\partial x}$$



It indicates the rate of increase or decrease in length of a fluid element in x-direction.

Similarly: $\epsilon_{yy} = \frac{\partial v}{\partial y}$, $\epsilon_{zz} = \frac{\partial w}{\partial z}$

ϵ_{xx} , ϵ_{yy} , ϵ_{zz} are called **linear strain rate**

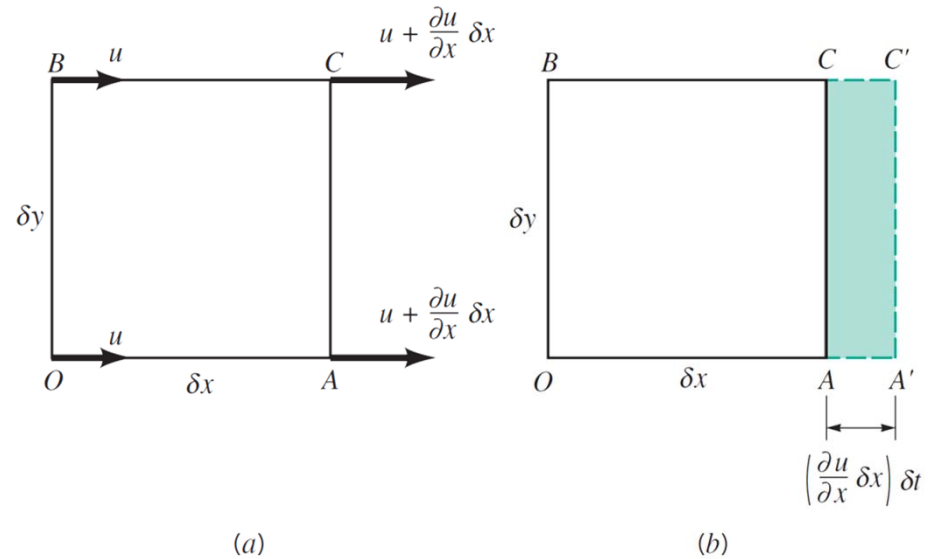




2.3 Deformation and Rotation of Fluid Elements

Apparently:
$$\varepsilon_{xx} + \varepsilon_{yy} + \varepsilon_{zz} = \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = \nabla \cdot \mathbf{V}$$

$\nabla \cdot \mathbf{V}$ is the **divergence of velocity**, denoting the rate of change of volume of a fluid element per unit volume (**volumetric strain/dilatation rate**).



Change of volume in x-direction:

$$\delta V_x = \left[\left(u + \frac{\partial u}{\partial x} \delta x \right) \delta y \cdot \delta z \cdot \delta t \right] - (u \cdot \delta y \cdot \delta z \cdot \delta t) = \frac{\partial u}{\partial x} \delta x \cdot \delta y \cdot \delta z \cdot \delta t$$

Change of volume in x-direction per unit volume per unit time:

$$\frac{\delta V_x}{V \cdot \delta t} = \frac{\frac{\partial u}{\partial x} \cdot \delta x \cdot \delta y \cdot \delta z \cdot \delta t}{\delta x \cdot \delta y \cdot \delta z \cdot \delta t} = \frac{\partial u}{\partial x} \text{ as } \delta x, \delta t \rightarrow 0$$



2.3 Deformation and Rotation of Fluid Elements

Similarly, in y and z directions:

$$\frac{\delta \mathcal{V}_y}{\mathcal{V} \cdot \delta t} = \frac{\partial v}{\partial y}, \quad \frac{\delta \mathcal{V}_z}{\mathcal{V} \cdot \delta t} = \frac{\partial w}{\partial z} \quad \text{as } \delta y, \delta z, \delta t \rightarrow 0$$

Thus, the total change of volume per unit volume per unit time is:

$$\frac{\delta \mathcal{V}}{\mathcal{V} \cdot \delta t} = \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = \nabla \cdot \mathbf{V} \quad \text{as } \delta x, \delta y, \delta z, \delta t \rightarrow 0$$

The **divergence of velocity** $\nabla \cdot \mathbf{V}$ can be used to express the **volumetric strain/dilatation rate**



$$\nabla \cdot \mathbf{V} = 0 \quad \Leftrightarrow \quad \text{Incompressible flow}$$



2.3 Deformation and Rotation of Fluid Elements

$\nabla \cdot \mathbf{V} > 0$, indicates the fluid flows **out** of the element and is called a **source** flow

$\nabla \cdot \mathbf{V} < 0$, indicates the fluid flows **into** the element and is called a **sink** flow

$\nabla \cdot \mathbf{V} = 0$, indicates the velocity field of the incompressible fluid is **without** the source flow.



上海交通大学

Shanghai Jiao Tong University

2.3 Deformation and Rotation of Fluid Elements

(2) Physical meaning of ε_{xy} , ε_{xz} , ε_{zy}

(3) Physical meaning of ω_x , ω_y , ω_z



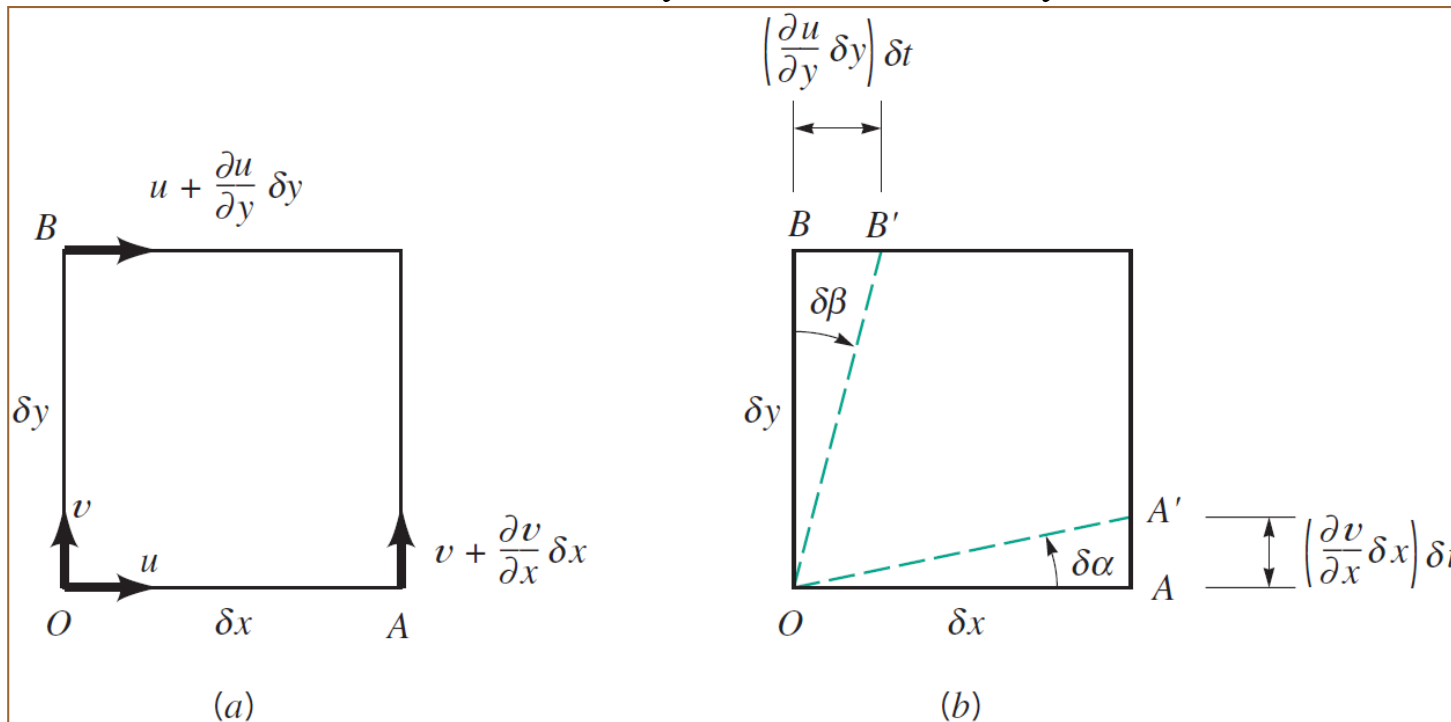
2.3 Deformation and Rotation of Fluid Elements

For a fluid element (in the x - y plane), the change of line **OA** in a short time interval δt is:

$$\delta\alpha = \text{tg}(\delta\alpha) = \frac{\partial v}{\partial x} \delta x \delta t / \delta x = \frac{\partial v}{\partial x} \delta t$$

Similarly,

$$\delta\beta = \text{tg}(\delta\beta) = \frac{\partial u}{\partial y} \delta y \delta t / \delta y = \frac{\partial u}{\partial y} \delta t$$





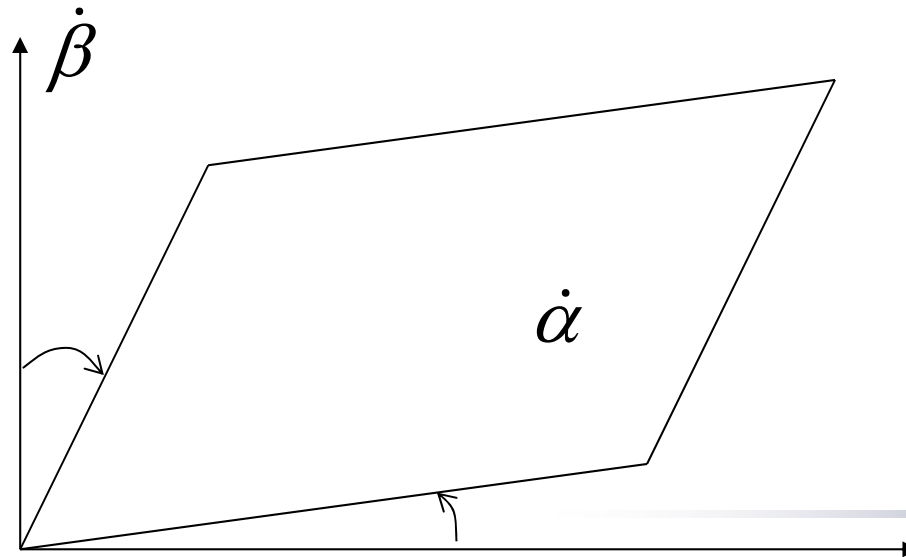
2.3 Deformation and Rotation of Fluid Elements

The **angular velocity** of line OA is:

$$\dot{\alpha} = \frac{d\alpha}{dt} = \frac{\partial v}{\partial x} \quad \text{as } \delta x, \delta t \rightarrow 0$$

Similarly, the **angular velocity** of line OB is:

$$\dot{\beta} = \frac{d\beta}{dt} = \frac{\partial u}{\partial y} \quad \text{as } \delta y, \delta t \rightarrow 0$$





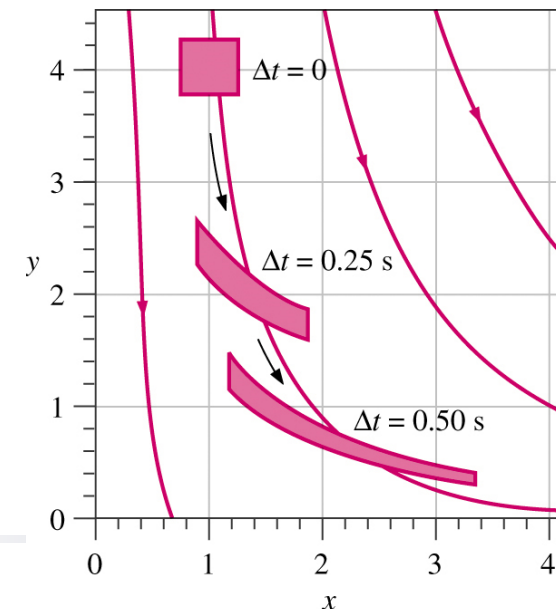
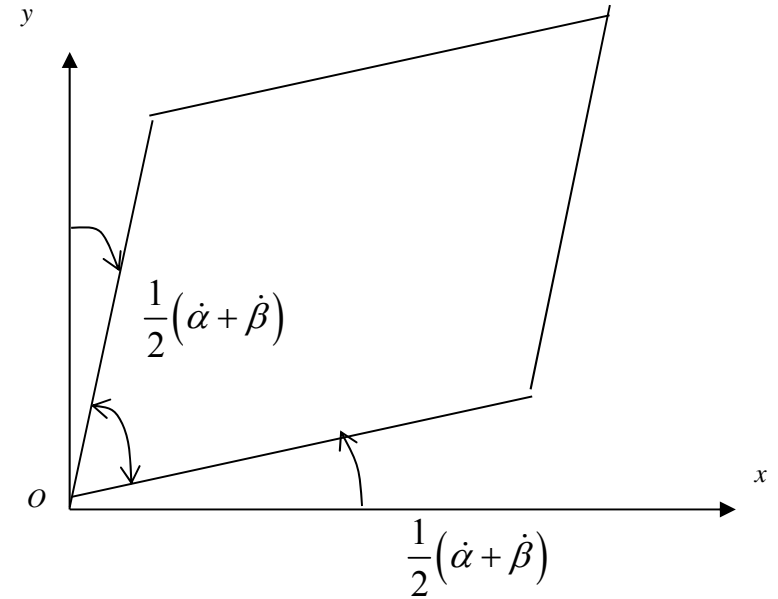
2.3 Deformation and Rotation of Fluid Elements

$$\therefore \varepsilon_{xy} = \frac{1}{2} \left(\frac{\partial v}{\partial x} + \frac{\partial u}{\partial y} \right) = \frac{1}{2} (\dot{\alpha} + \dot{\beta})$$

It denotes the **rate of angular deformation** of a right angle in the fluid element, it is called **shear strain rate**. When $\varepsilon_{xy} > 0$, the angle decreases;
In contrast, the angle increases.

Similarly:

$$\varepsilon_{yz} = \frac{1}{2} \left(\frac{\partial w}{\partial y} + \frac{\partial v}{\partial z} \right)$$
$$\varepsilon_{zx} = \frac{1}{2} \left(\frac{\partial u}{\partial z} + \frac{\partial w}{\partial x} \right)$$

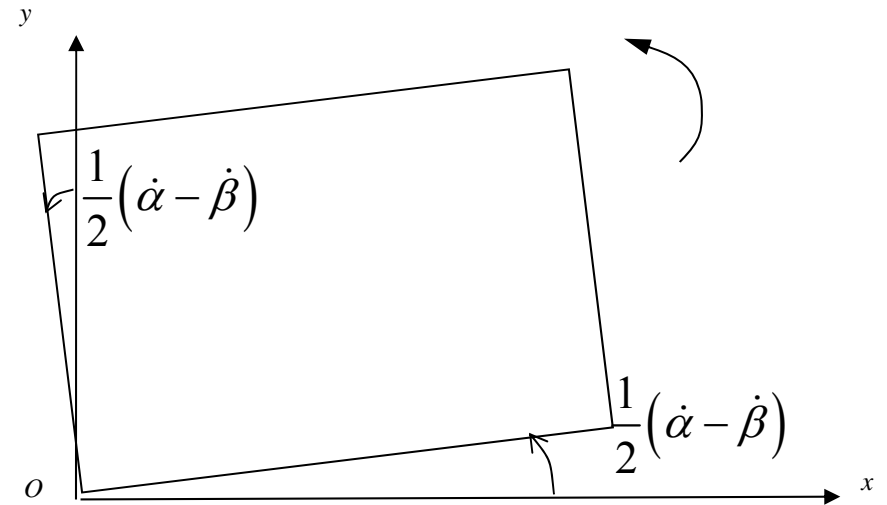




2.3 Deformation and Rotation of Fluid Elements

$$\omega_z = \frac{1}{2}(\dot{\alpha} - \dot{\beta}) = \frac{1}{2}\left(\frac{\partial v}{\partial x} - \frac{\partial u}{\partial y}\right)$$

It denotes the **rate of rotation**, **angular velocity** of the fluid element. When $\omega_z > 0$, the fluid element rotates in **counterclockwise** direction; in contrast, it rotates in **clockwise** direction.



Similarly:

$$\omega_x = \frac{1}{2}\left(\frac{\partial w}{\partial y} - \frac{\partial v}{\partial z}\right), \quad \omega_y = \frac{1}{2}\left(\frac{\partial u}{\partial z} - \frac{\partial w}{\partial x}\right)$$



2.3 Deformation and Rotation of Fluid Elements

$$\mathbf{V}_{M'} = \left[\underbrace{\mathbf{u}}_{(1)} + \underbrace{\omega_z dy + \omega_y dz}_{(2)} + \underbrace{\epsilon_{xx} dx}_{(3)} + \underbrace{\epsilon_{xy} dy + \epsilon_{xz} dz}_{(4)} \right] \mathbf{i} + (\dots)\mathbf{j} + (\dots)\mathbf{k}$$

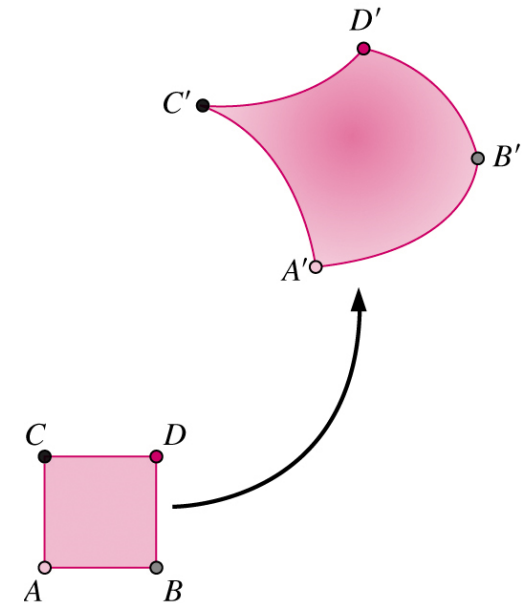
General motion = {

- Translation (1)
- +
- Rotation (2)
- +
- Dilatation (3)
- +
- Angular deformation (4)

(rigid body motion)

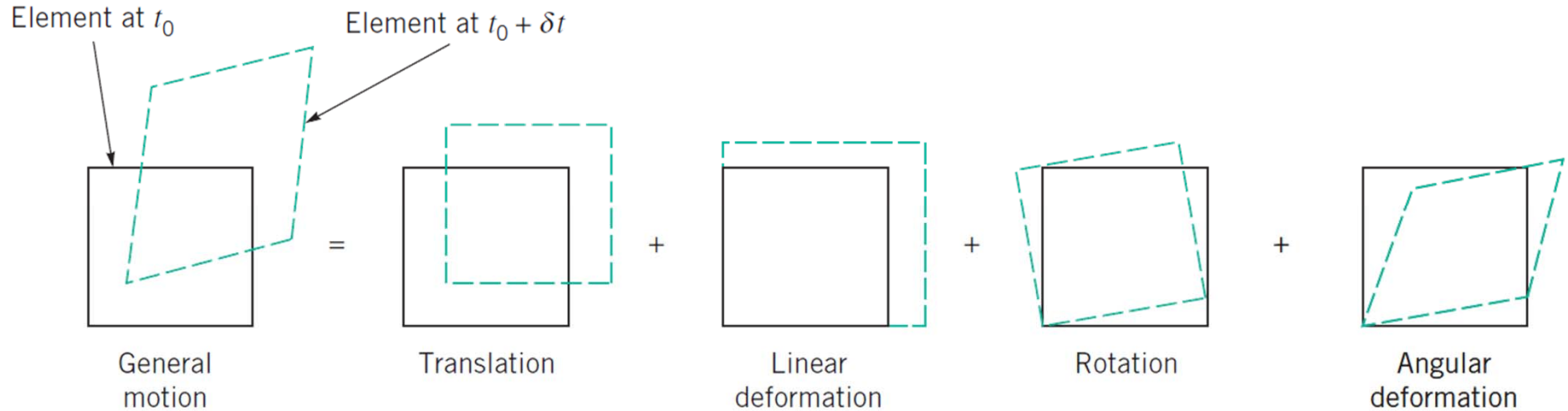
(change in volume)

(change in shape)





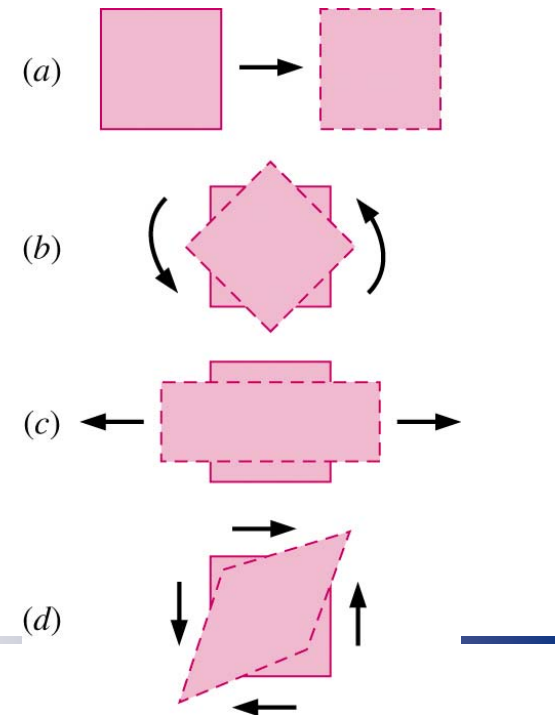
2.3 Deformation and Rotation of Fluid Elements



Helmholtz velocity decomposing theorem:

An fluid element may undergo **four** fundamental types of motion or deformation:

- (a) translation,
- (b) rotation,
- (c) linear strain,
- and (d) shear strain



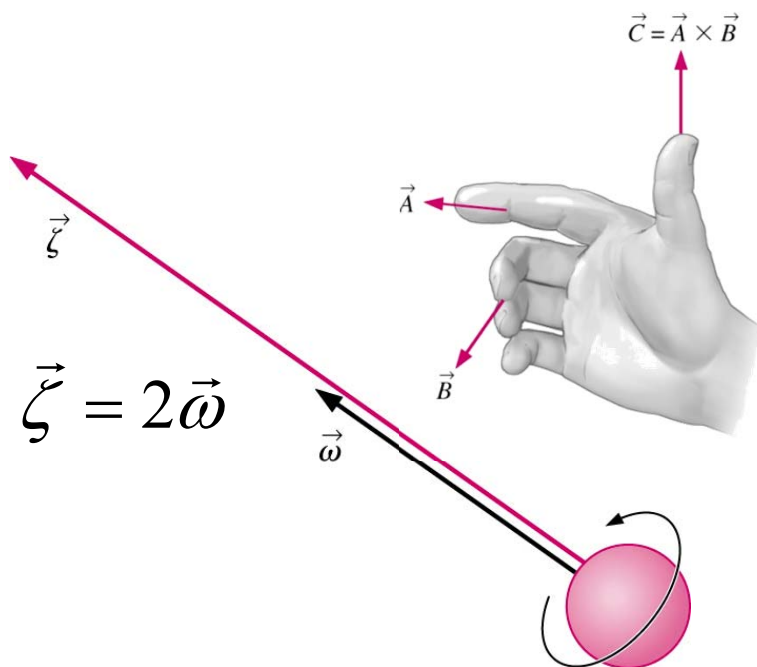


2.3 Deformation and Rotation of Fluid Elements

shear rate tensor $\mathbf{E} = e_{ij} = \frac{1}{2} \left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right)$

rate of rotation $\boldsymbol{\omega} = \omega_x \vec{i} + \omega_y \vec{j} + \omega_z \vec{k} = \frac{1}{2} \boldsymbol{\zeta}$ (vorticity)

vorticity $\boldsymbol{\zeta} = \boldsymbol{\Omega} = \nabla \times \mathbf{V}$ (curl of velocity)



$$= \begin{vmatrix} \vec{i} & \vec{j} & \vec{k} \\ \frac{\partial}{\partial x} & \frac{\partial}{\partial y} & \frac{\partial}{\partial z} \\ u & v & w \end{vmatrix}$$

$$= \underbrace{\left(\frac{\partial w}{\partial y} - \frac{\partial v}{\partial z} \right)}_{2\omega_x} \vec{i} + \underbrace{\left(\frac{\partial u}{\partial z} - \frac{\partial w}{\partial x} \right)}_{2\omega_y} \vec{j} + \underbrace{\left(\frac{\partial v}{\partial x} - \frac{\partial u}{\partial y} \right)}_{2\omega_z} \vec{k}$$