第三次作业

作业题目在交大 public网站上:

目录名:船舶流体力学作业2015

文件名: Exercise-2015-03.pdf

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● 在4月13日提交作业。



速度势

无旋
$$\Leftrightarrow \nabla \times \mathbf{v} = \mathbf{o} \Leftrightarrow \phi \Leftrightarrow$$
势流

$$\phi(x, y, z; t) = \int u dx + v dy + w dz$$

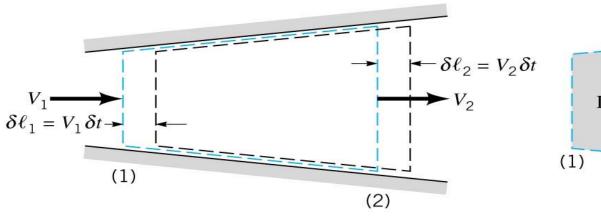
$$\frac{\partial \phi}{\partial x} = u$$

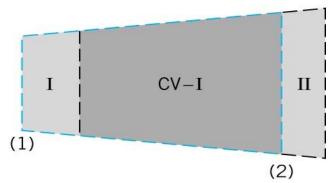
$$\mathbf{V} = \nabla \phi, \qquad \frac{\partial \phi}{\partial y} = v$$

$$\frac{\partial \phi}{\partial z} = w$$



• 系统与控制体





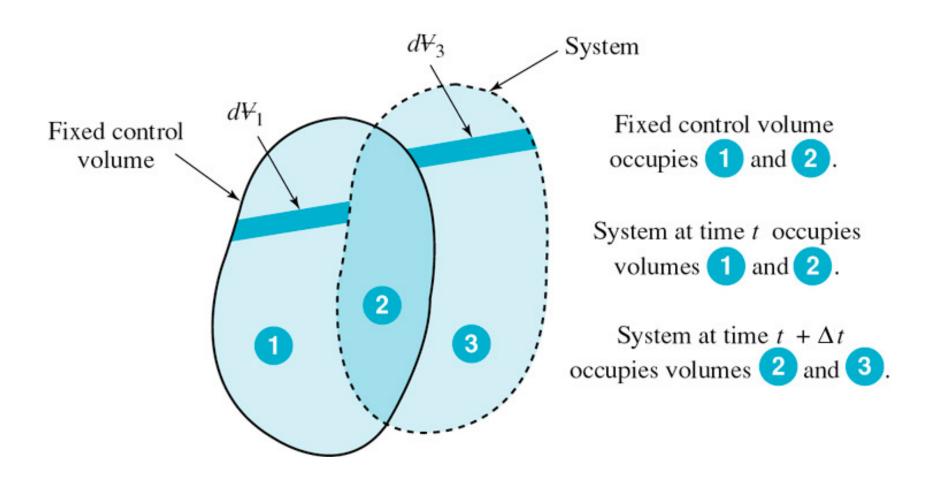
- Fixed control surface and system boundary at time t
- --- System boundary at time $t + \delta t$

(a)

(b)

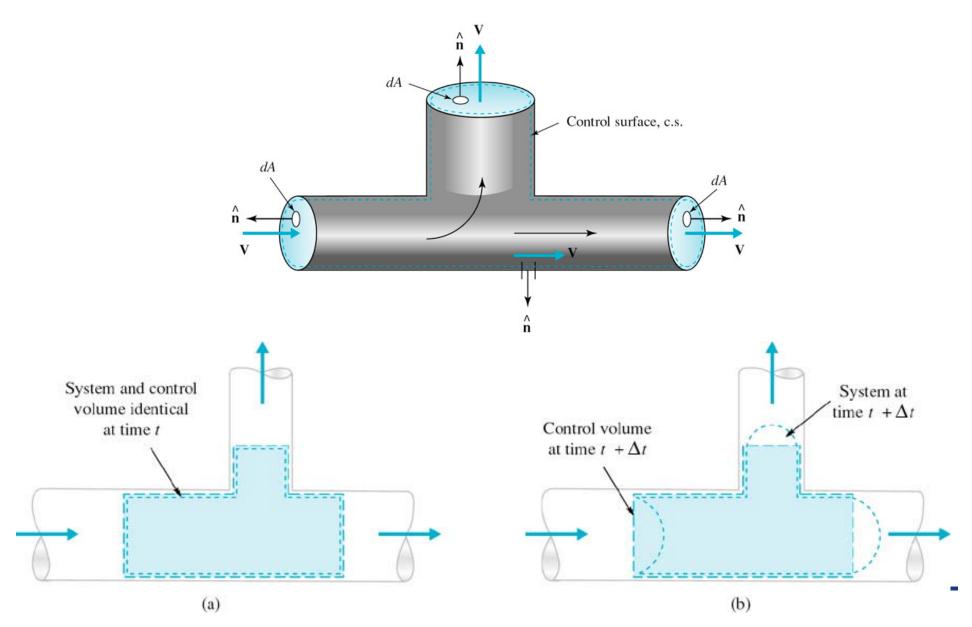






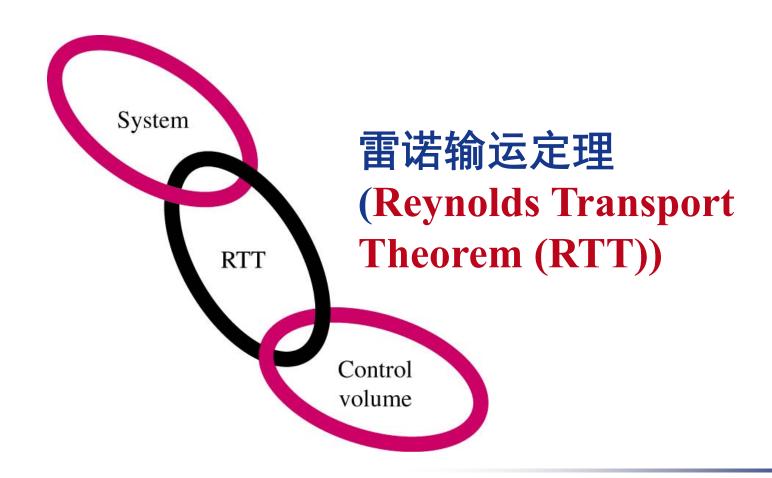


复习





流体动力学的两个研究途径: 系统途径和控制体途径。



3.2 雷诺输运定理

雷诺输运定理(Reynolds Transport Theorem)

任何一个物理量*G*都满足下列<u>物质体积</u>与<u>控</u>制体积的关系式:

$$\frac{d}{dt} \iiint_{MV} \mathbf{G} dV = \frac{\partial}{\partial t} \iiint_{CV} \mathbf{G} dV + \iint_{CS} \mathbf{G} \mathbf{V} \cdot \mathbf{n} dA$$

rate of change of the property within the material volume

local rate of change of the property within the fixed control volume that happens to coincide with the material volume at that instant net out-flux of the property across the entire control surface

 ρ = density of fluid

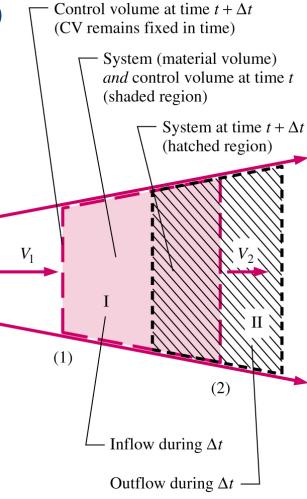
G = an intensive property of fluid

MV = material volume that happens to coincide with CV at time t

CV = control volume (fixed in space)

CS = control surface

 \mathbf{n} = unit outward normal to *CS*



At time t: Sys = CV At time $t + \Delta t$: Sys = CV – I + II

3.2 雷诺输运定理

对于物质体,在dt后为:

$$\left[\iiint_{MV} G(\mathbf{x},t) dV\right]_{t+dt} = \iiint_{MV(t+dt)} G(\mathbf{x},t+dt) dV = \iiint_{MV(t+dt)} \left[G(\mathbf{x},t) + \frac{\partial G}{\partial t} dt + O(dt)^{2}\right] dV$$

在
$$dt$$
内物质体的变化为: $\iiint_{MV(t+dt)} () = \iiint_{MV} () + \iiint_{\Delta V} () = \iiint_{CV} () + \iiint_{CS} () \mathbf{V} \cdot \mathbf{n} dS dt$

因此有:

$$\left[\iiint_{MV} G(\mathbf{x}, t) dV \right]_{t+dt} = \iiint_{MV(t+dt)} \left[G(\mathbf{x}, t) + \frac{\partial G}{\partial t} dt \right] dV$$

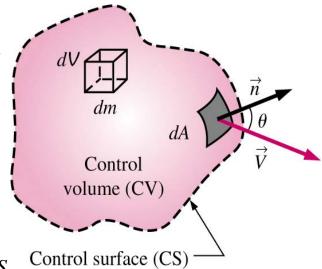
$$= \iiint_{CV} \left[G(\mathbf{x}, t) + \frac{\partial G}{\partial t} dt \right] dV + \iint_{CS} \left[G(\mathbf{x}, t) + \frac{\partial G}{\partial t} dt \right] \mathbf{V} \cdot \mathbf{n} dS dt$$

$$= \iiint_{CV} G(\mathbf{x}, t) dV + \left[\iiint_{CV} \frac{\partial G}{\partial t} dV + \iint_{CS} G(\mathbf{x}, t) \mathbf{V} \cdot \mathbf{n} dS \right] dt$$

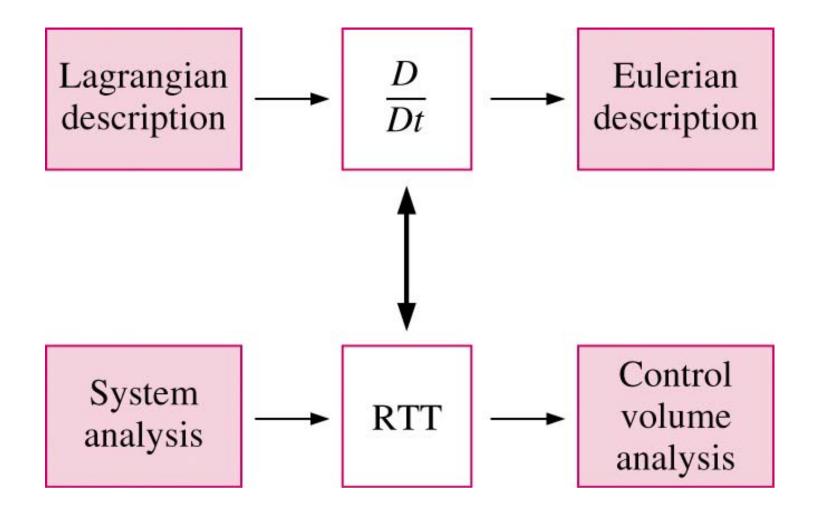
由上式可以得到RTT:

$$\frac{d}{dt} \iiint_{MV} G dV = \left\{ \left[\iiint_{MV} G dV \right]_{t+dt} - \iiint_{MV} G dV \right\} \middle/ dt = \iiint_{CV} \frac{\partial G}{\partial t} dV + \iint_{CS} G \mathbf{V} \cdot \mathbf{n} dS$$

删去二阶小量



3.2 雷诺输运定理



连续方程(Continuity Equation): 也称为质量守恒方程 (Conservation of Mass)

在RTT方程中,如果物理量为质量,即 $G = \rho$,可以得到:

L.H.S.
$$\frac{d}{dt} \iiint_{MV} \rho dV = \frac{d}{dt} (\text{mass in } MV) = 0$$

(由 MV的定义:在MV中总是包含相同的流体。)

R.H.S.
$$\frac{\partial}{\partial t} \iiint_{CV} \rho dV + \iint_{CS} \rho V \cdot n dA$$
$$= \iiint_{CV} \frac{\partial \rho}{\partial t} dV + \iiint_{CV} \nabla \cdot (\rho V) dV$$
by Gauss theorem

由于控制体积CV是任一选取的,因此可以得到:

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{V}) = 0$$

这就是连续方程。进一步,可以把上式改写:

把 $\nabla \cdot (\rho \mathbf{V}) = \mathbf{V} \cdot \nabla \rho + \rho \nabla \cdot \mathbf{V}$ 代入上式,可以得到:

$$\frac{\partial \rho}{\partial t} + \mathbf{V} \cdot \nabla \rho + \rho \nabla \cdot \mathbf{V} = \frac{D\rho}{Dt} + \rho \nabla \cdot \mathbf{V} = 0$$

或
$$\frac{D\rho}{Dt} + \rho \frac{\partial u_i}{\partial x_i} = 0$$

对于不可压缩流体(incompressible fluid), 我们知道:

the density of a fluid particle is invariant with time $\Leftrightarrow \frac{D\rho}{Dt} = 0$

$$\Leftrightarrow \frac{D\rho}{Dt} = 0$$

因此,对应不可压缩流体,连续方程为:

$$\nabla \cdot \mathbf{V} = 0$$

(ie, divergence of velocity is zero for incompressible flow)

即:

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0$$

也可以从质量守恒的角度来得到连续方程。在流场中任取一流 域 Ω . 其表面积为S. 此时质量守恒定律的描述为:

流体质量增加(减少) = 单位时间内流进(流出)S的质量流量

$$\frac{\partial}{\partial t} \iiint_{\Omega} \rho \, d\Omega = - \oiint_{S} \rho (\mathbf{V} \cdot \mathbf{n}) ds = - \iiint_{\Omega} \nabla \cdot (\rho \mathbf{V}) d\Omega$$



$$\iiint_{\Omega} \left[\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{V}) \right] d\Omega = 0$$
 (积分形式连续方程)

由于Ω是任取的,所以有:

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{V}) = 0$$
 (微分形式连续方程)



$$\frac{D\rho}{Dt} + \rho \nabla \cdot \mathbf{V} = 0$$

由于可以从质量守恒推导得到,因此连续方程也称为质量守恒方程。无论理想流体还是真实流体,均应满足连续方程,否则流动为不可能。

连续方程的几种不同表达形式:

可压缩不定常流动:
$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{V}) = 0$$

可压缩定常流动:
$$\nabla \cdot (\rho \mathbf{V}) = 0$$

不可压缩不定常流动:
$$\nabla \cdot \mathbf{V} = \mathbf{0}$$

不可压缩定常流动:
$$\nabla \cdot \mathbf{V} = 0$$



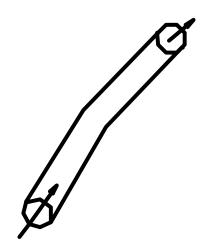
流管流动:

如果S1、S2为流管横截面积,V1、ρ1

- 、V2、ρ2为横截面上平均流速和密度
- ,则质量守恒方程或连续方程为:

$$\rho_1 \mathbf{V}_1 S_1 = \rho_2 \mathbf{V}_2 S_2$$
or
$$\rho \mathbf{V} S = const$$

对于不可压流 :
$$\mathbf{V}_1 S_1 = \mathbf{V}_2 S_2$$



例子 一个三维不可压流场速度分布为 $u = x^2 y$, $v = 4y^3 z$, w = 2z 问这个流动是否是一个真实流动?

解: 不可压流体的真实流动必须满足连续条件,即:

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0$$

对于给出的速度场,有:

$$\frac{\partial u}{\partial x} = 2xy$$
, $\frac{\partial v}{\partial y} = 12y^2z$, $\frac{\partial w}{\partial z} = 2$

可以看出:

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 2 x y + 1 2 y^2 z + 2 \neq 0$$

因此这个速度场不是一个真实的流动。



- 速度势 (velocity potential)
 - ——针对无旋运动流体。

- · 流函数 (stream function)
 - —— 针对不可压缩流体。

定理:

如果函数 P(x,y), Q(x,y) 在封闭区域及其边界上具有一阶连续偏导数,则曲线积分 $\int P dx + Q dy$ 与路径无关之必要且充分条件是 $\frac{\partial P}{\partial y} = \frac{\partial Q}{\partial x}$ 。

根据连续方程可知:对于不可压平面二维流动满足:

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \qquad \qquad \frac{\partial u}{\partial x} = \frac{\partial}{\partial y} (-v)$$

如果令 P = -v, Q = u, 则存在一积分函数:

$$\psi = \int Pdx + Qdy = \int -vdx + udy$$

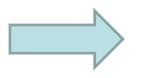
与路径无关, $\Psi = (x, y, t)$ 称为流函数(stream function)。



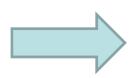
$$\psi = \int -v dx + u dy$$

$$\int d\psi = \int -v dx + u dy$$

$$\int d\psi = \int -vdx + udy$$



$$\int \frac{\partial \psi}{\partial x} dx + \frac{\partial \psi}{\partial y} dy = \int -v dx + u dy$$



$$\begin{cases} \frac{\partial \psi}{\partial x} = -v \\ \frac{\partial \psi}{\partial y} = u \end{cases}$$

流函数存在条件:

对于理想或真实流体,只要是不可压流的二元流,均存在流 函数;

对于可压流体平面流动,只要流动是定常的,也同样存在流 函数:

$$\frac{\partial \rho u}{\partial x} + \frac{\partial \rho v}{\partial y} = 0 \qquad \qquad \frac{\partial \rho u}{\partial x} = \frac{\partial}{\partial y} (-\rho v)$$

$$\psi = \int -\rho v dx + \rho u dy$$

$$\begin{cases} \rho u = \frac{\partial \psi}{\partial y} \\ -\rho v = \frac{\partial \psi}{\partial x} \end{cases}$$



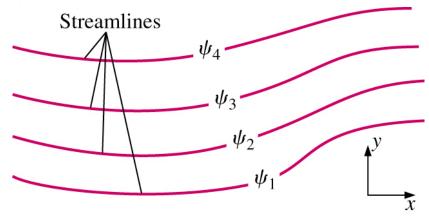
流函数的一些性质:

1) 流函数与流线关系:流函数的等值线是流线,即流线上的流函数值不变。

由于:
$$d\psi = \frac{\partial \psi}{\partial x} dx + \frac{\partial \psi}{\partial y} dy = -v dx + u dy$$

所以,若
$$\Psi = \mathbf{c}$$
 则 $\frac{dx}{u} = \frac{dy}{v}$ 即代表流线方程。

注意:流函数仅存在于连续方程只 含平面二维的流动中,而流线存在 所有可能流动中。



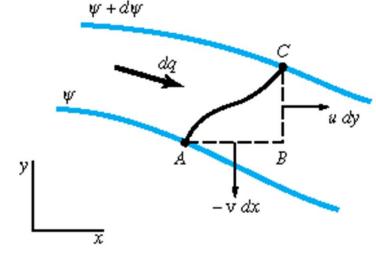
2) 流函数Ψ与流量Q关系

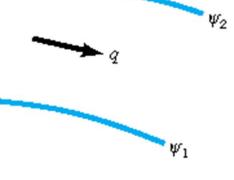
流过任意曲线的流量,等于曲线两端点流函数值之差,

即 $Q_{AC} = \psi_C - \psi_A$ (**Y**为单值函数)。

$$dq = udy - vdx = \frac{\partial \psi}{\partial y}dy + \frac{\partial \psi}{\partial x}dx = d\psi$$

$$\therefore q = \int_{\psi_1}^{\psi_2} d\psi = \psi_2 - \psi_1$$





3) <u>不可压无旋二维</u>势流的速度势和流函数都是调和函数,满足 Laplace方程。

A、不可压(二)三维势流(无旋)

无旋 ⇒
$$\nabla \times \mathbf{V} = 0$$
 ⇒ $\mathbf{V} = \nabla \phi$ ⇒ $\nabla \cdot \mathbf{V} = 0$ \Rightarrow $\nabla^2 \phi = 0$

B、不可压二维势流(无旋)

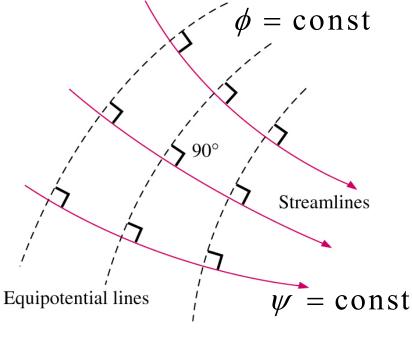
二维不可压
$$\Rightarrow$$
 $u = \frac{\partial \psi}{\partial y}, v = -\frac{\partial \psi}{\partial x}$ \Rightarrow $\nabla^2 \psi = 0$
二维无旋 $\Rightarrow \frac{\partial v}{\partial x} - \frac{\partial u}{\partial y} = 0$

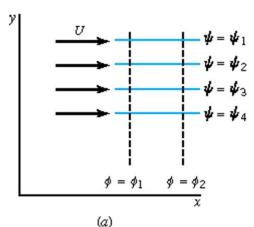
4) 流网线(flow net): 是由二维不可压势流的流线(streamlines) 和等势线(equipotential lines)组成的交叉格子线。

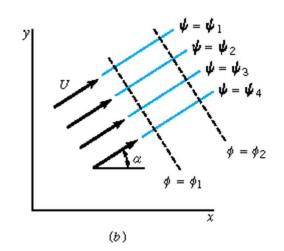
$$\nabla \phi \equiv V$$

 $\nabla \phi \equiv V$ \perp equipotential lines

streamlines \(\preceq \) equipotential lines









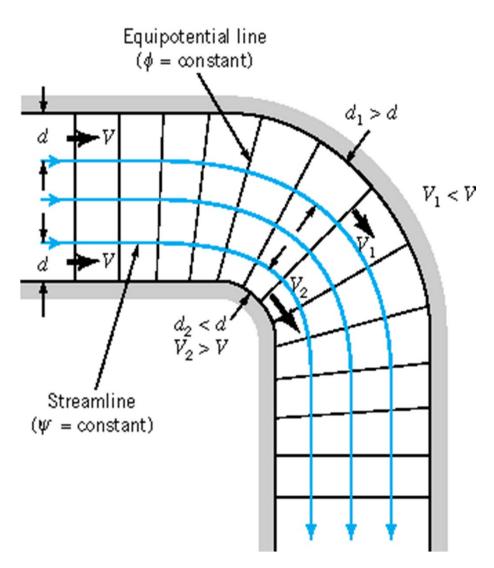
对于一个900弯管,有:

$$V \approx \frac{\Delta \phi}{\Delta n} \approx \frac{\Delta \psi}{\Delta s}$$

 Δn 是邻近两条等势线的距离。

 Δs 是邻近两条流线的距离。

流网线密,表示流速大;流网线疏,表示流速小。



例题:假设速度分布如下,试求Ψ及流线族。

$$u = \frac{m}{2\pi} \frac{x}{x^2 + y^2}, \quad v = \frac{m}{2\pi} \frac{y}{x^2 + y^2}$$

解: 首先验证Ψ是否存在,即 $\nabla \cdot \mathbf{V} = 0$

$$\nabla \cdot \mathbf{V} = \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = \frac{m}{2\pi} \cdot \left[\frac{y^2 - x^2}{(x^2 + y^2)^2} + \frac{x^2 - y^2}{(x^2 + y^2)^2} \right] = 0$$

满足 Ψ 存在条件,下面求 Ψ

$$\psi = \int -v dx + u dy = \int -\frac{m}{2\pi} \frac{y}{x^2 + y^2} dx + \frac{m}{2\pi} \frac{x}{x^2 + y^2} dy$$

$$= \frac{m}{2\pi} \int \frac{x dy - y dx}{x^2 + y^2} = \frac{m}{2\pi} \int \frac{d(y/x)}{1 + (\frac{y}{x})^2}$$

$$=\frac{m}{2\pi}tg^{-1}\frac{y}{x}+c$$

也可以用另一种方法解:

$$\therefore \frac{\partial \psi}{\partial y} = u = \frac{m}{2\pi} \frac{x}{x^2 + y^2}$$

$$\therefore \psi = \int u \, dy = \frac{m}{2 \pi} \int \frac{x}{x^2 + y^2} \, dy$$

$$= \frac{m}{2\pi} \int \frac{d^{-\frac{y}{x}}}{1 + (y/x)^{2}} = \frac{m}{2\pi} t g^{-1} (y/x) + f(x)$$

$$\frac{\partial \psi}{\partial x} = -v, \quad \mathbb{R} \frac{m}{2\pi} \frac{-\frac{y}{x^2}}{1 + (\frac{y}{x})^2} + f'(x) = -\frac{m}{2\pi} \frac{y}{x^2 + y^2}$$

$$f'(x) = 0$$
, $\mathbb{P} f(x) = c \implies \psi = \frac{m}{2\pi} t g^{-1}(\frac{y}{x})$

例子2 已知一个流场速度势, $\phi = 4xy$, 求其对应的流函数。

解: 由速度势,可以得到速度分布:

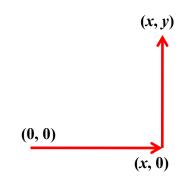
$$u = \frac{\partial \phi}{\partial x} = 4y, \qquad v = \frac{\partial \phi}{\partial y} = 4x$$

从上式,得到: $\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$, 因此存在流函数。

由流函数定义,有:

$$\psi = \int -v dx + u dy = \int -4x dx + 4y dy$$

$$= \int_{(0,0)}^{(x,0)} + \int_{(x,0)}^{(x,y)} = -2x^2 + 2y^2 + C$$



这里C是常数。